

Notified Body 1880 – Regulation (EU) no305/2011

TEST REPORT n.1880-CPR-004-17

## Compliance of dust load to European Regulations (Austrian 15a B-VG, German BIMSChv, French Flamme Verte and Swiss LRV)

Residential space heating appliances fired by wood pellets  
UNI EN 14785:2006

Manufacturer: KLOVER SRL  
Via A. Volta, 8  
37047 SAN BONIFACIO (VR)  
Italy

Type designation: PFP 18 - prototype

Type of appliance: Residential space heating appliances fired by wood pellets with water heat exchanger with direct and indirect water system.

Receipt date: February 10, 2017

Start test date: February 14, 2017

End test date: February 20, 2017

Testing laboratory: ACTECO SRL  
via Amman, 41  
33084 Cordenons (PN)  
Italy

Issue date: April 28, 2017

Head of Test Laboratory  
Dr. Claudia Marcuzzi

The results of the tests relate only to the tested appliance.  
This test report shall not be reproduced except in full, without written approval of the laboratory.  
The appliance was returned to the manufacturer after the end of tests.  
All data is stored for 10 years  
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## Task

ACTECO SRL was instructed to execute initial type testing to establish compliance according to the:

- European standard UNI EN 14785:2006 Residential space heating appliances fired by wood pellets
- UNI CEN/TS 15883:2009 Residential solid fuel burning appliances. Emission test methods
- Client's documents

The practical tests were performed in the laboratory in Cordenons (PN), via Amman, 41.

## Sampling of the appliance

The sampling of the appliance was performed by the manufacturer and was received by the testing laboratory on February 10, 2017.

## Description of the appliance

Residential space heating appliances fired by wood pellets with direct and indirect water system.  
The combustion air is taken from the test room.

### Key data of appliance

Appliance	PFP 18	
Fuel		Wood pellet
Fuel throughput	kg/h	3,41
Total heating output	kW	15,8
Space heating output	kW	3,5
Water heating output	kW	12,3
CO emission based on 13% O <sub>2</sub>	mg/m <sup>3</sup>	127
Efficiency	%	93,6
Flue gas temperature	°C	135,4
Necessary flue draught	Pa	9,9
Flue gas mass flow	g/s	7,8
Permissible maximum operating pressure	bar	2,5
Minimum clearance distances from exposed / combustibile materials	from rear wall from side walls	150 mm 150 mm

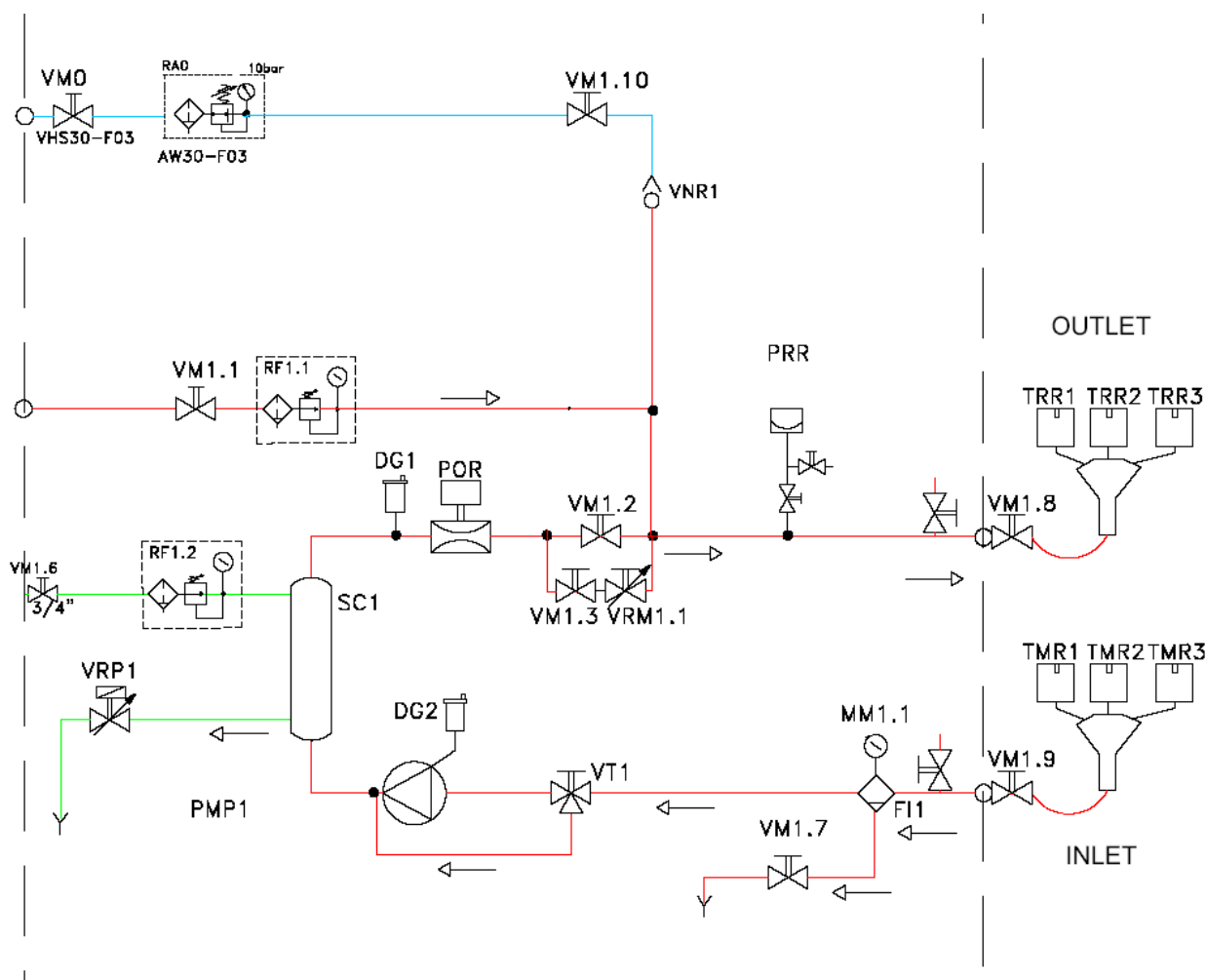
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### Description of the water circuit used for the water heating output test

The water circuit used for the water heating output test was a closed circuit as shown in the figure below. The outlet temperature was set to  $80^{\circ}\text{C} \pm 5^{\circ}\text{C}$  and the water flow was set to a constant flow according to the expected boiler heat output. During the test period, inlet and outlet temperatures and the water flow were measured at 10 second intervals. At the end of the test period, the mean rise in water temperature between boiler inlet and outlet and the mean water flow were calculated.



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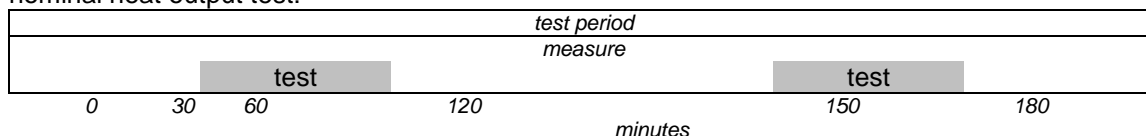
## Description of the dust emission test

Measurement of particulate emissions is performed with UNI CEN/TS 15883:2009 (equivalent to VDI 2066:2006 part 1) parallel to CO-measurement during the initial type testing according to the nominal heat output test described in UNI EN 14785:2006 A.4.7.

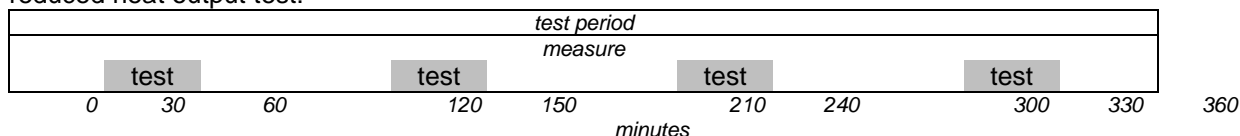
A sample flow of the gas is extracted from the main gas flow at a representative sampling point for the sampling period with a controlled flow rate and the withdrawn volume is measured. The dust entrained in the gas sample is separated by a pre-weighted plain quartz fibre filter, which is dried and re-weighted. The increase of mass of the filter is attributed to the dust collected from the sampled gas.

The measurement position for particle measurement is arranged downstream of measurement positions of CO, CO<sub>2</sub>, NO<sub>x</sub> and OGC (Organic Gaseous Compounds). Measurement of particulate emissions and duration of measurements are described in the following scheme.

nominal heat output test:



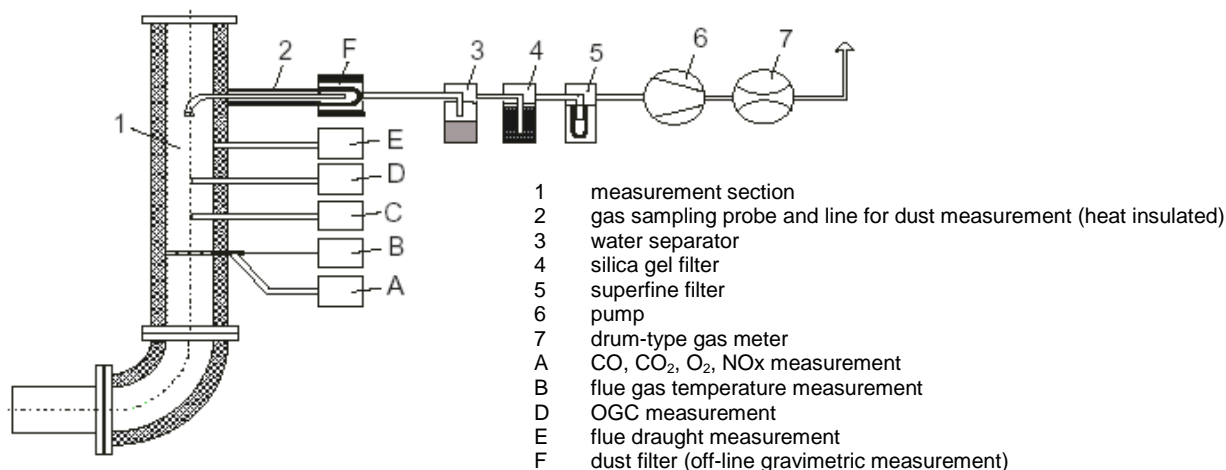
reduced heat output test:



The measuring arrangement is illustrated in the following figure. The sampling tube widens out to 9,74 mm at the specimen inlet. In a sampling period of 30 minutes a waste gas volume of  $270 \pm 13,5$  l relative to normal conditions (273 K, 1013 hPa) is sampled, corresponding to a flow rate of  $10,0 \pm 0,45$  l/min.

*Note: In the interests of simplifying the measuring method, individual measurement of the flow velocity and subsequent matching of the inlet cross-section are dispensed with. In order to carry out the measurement, the sampling probe is centred in the exhaust-gas cross-section..*

The measuring filter is inserted in a filter holder at the end of the sampling probe and a controlled probe heating system is adopted to exclude the possibility of the sampled flue gas falling below the dew point in front of or in the filter sleeve.



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## PERFORMANCE AT THE NOMINAL HEAT OUTPUT TEST

test n°		1	2	average
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Combustion:					
fuel load		<i>kg</i>	10,1	10,3	10,2
test period		<i>min</i>	180	180	180
fuel load	<i>B</i>	<i>kg/h</i>	3,37	3,45	3,41
average flue draught		<i>Pa</i>	9,9	9,8	9,9

Ventilation circuit:					
average ambient room temperature	<i>tr</i>	<i>°C</i>	18,6	20,9	19,8

Flue gas:					
carbon dioxide	<i>CO<sub>2</sub></i>	<i>%</i>	14,0	14,1	14,1
oxygen	<i>O<sub>2</sub></i>	<i>%</i>	7,3	7,3	7,3
carbon monoxide	<i>CO</i>	<i>%</i>	0,017	0,018	0,018
average flue gas temperature	<i>ta</i>	<i>°C</i>	134,6	136,2	135,4
maximum flue gas temperature		<i>°C</i>	137,4	138,3	137,9
flue gas mass flow	<i>m</i>	<i>g/s</i>	7,7	7,8	7,8

Maximum surface temperatures:					
charging door handle (metal)		<i>°C</i>	101,3	106,0	103,7
internal fuel hopper		<i>°C</i>	55,5	56,5	56,0
conveyor system where there is pellet		<i>°C</i>	55,5	57,3	56,4

Maximum trihedron surface temperatures:					
hearth		<i>°C</i>	23,8	25,8	24,8
side wall		<i>°C</i>	35,8	36,0	35,9
back wall		<i>°C</i>	27,0	28,6	27,8

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test n°			1	2	average
Results:					
thermal losses in flue gas	$q_a$	%	6,2	6,1	6,2
thermal losses in flue gas	$Q_a$	$kJ/kg$	1103	1090	1097
chemical losses in flue gas	$q_b$	%	0,07	0,08	0,08
chemical losses in flue gas	$Q_b$	$kJ/kg$	13,0	14,1	13,6
heat losses due to combustibile through the grate	$q_r$	%	0,2	0,2	0,2
efficiency	$\eta$	%	93,6	93,6	93,6
carbon monoxide [at 13% O <sub>2</sub> ]		%	0,010	0,011	0,010
carbon monoxide		$mg/MJ$	81	88	84
carbon monoxide [at 13% O <sub>2</sub> ]		$mg/m^3$	121	132	127
average boiler water output temperature		°C	76,8	77,2	77,0
average boiler water input temperature		°C	60,1	62,2	61,2
average boiler water temperature rise	$N$	°C	16,7	15,0	15,9
water flow rate	$M_w$	$kg/h$	624	690	657
water heat output	$P_w$	$kW$	12,3	12,3	12,3
space heat output	$P_{SH}$	$kW$	3,4	3,7	3,5
total heat output	$P$	$kW$	15,7	16,0	15,8

Dust emission: test A		$mg/MJ$	5,8	12,8	9,3
test B		$mg/MJ$	12,8	12,5	12,7
average		$mg/MJ$	9,3	12,7	11,0
Dust emission (at 13% O <sub>2</sub> ): test A		$mg/m^3$	8,7	19,3	14,0
test B		$mg/m^3$	19,3	18,8	19,1
average		$mg/m^3$	14,0	19,0	16,5
NOx		$ppm$	99	99	99
NOx (as NO <sub>2</sub> )		$mg/MJ$	79	78	79
NOx (as NO <sub>2</sub> at 13% O <sub>2</sub> )		$mg/m^3$	119	118	118
THC (as propane)		$ppm$	1,2	0,6	0,9
OGC (as C)		$mg/MJ$	0,8	0,4	0,6
OGC (as C at 13% O <sub>2</sub> )		$mg/m^3$	1,2	0,7	1,0

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## PERFORMANCE AT REDUCED HEAT OUTPUT TEST

test n°			1	2	average
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Combustion:					
fuel load		<i>kg</i>	5,6	5,5	5,6
test period		<i>min</i>	360	360	360
fuel load	<i>B</i>	<i>kg/h</i>	0,94	0,91	0,92
average flue draught		<i>Pa</i>	6,5	6,5	6,5

Ventilation circuit:					
average ambient room temperature	<i>tr</i>	<i>°C</i>	18,5	16,7	17,6

Flue gas:					
carbon dioxide	<i>CO<sub>2</sub></i>	<i>%</i>	7,9	8,4	8,1
oxygen	<i>O<sub>2</sub></i>	<i>%</i>	13,2	12,7	12,9
carbon monoxide	<i>CO</i>	<i>%</i>	0,055	0,050	0,053
average flue gas temperature	<i>ta</i>	<i>°C</i>	58,5	57,5	58,0
maximum flue gas temperature		<i>°C</i>	59,8	59,5	59,7
flue gas mass flow	<i>m</i>	<i>g/s</i>	3,9	3,5	3,7

Maximum surface temperatures:					
charging door handle (metal)		<i>°C</i>	73,9	72,7	73,3
internal fuel hopper		<i>°C</i>	53,4	53,2	53,3
conveyor system where there is pellet		<i>°C</i>	50,3	49,6	50,0

Maximum trihedron surface temperatures:					
hearth		<i>°C</i>	20,5	23,1	21,8
side wall		<i>°C</i>	30,1	28,4	29,3
back wall		<i>°C</i>	22,8	21,0	21,9

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test n°			1	2	average
Results:					
thermal losses in flue gas	$q_a$	%	3,5	3,4	3,5
thermal losses in flue gas	$Q_a$	$kJ/kg$	624	603	614
chemical losses in flue gas	$q_b$	%	0,4	0,4	0,4
chemical losses in flue gas	$Q_b$	$kJ/kg$	76	65	71
heat losses due to combustible through the grate	$q_r$	%	0,2	0,2	0,2
efficiency	$\eta$	%	95,9	96,1	96,0
carbon monoxide [at 13% O <sub>2</sub> ]		%	0,056	0,048	0,052
carbon monoxide		$mg/MJ$	468	399	434
carbon monoxide [at 13% O <sub>2</sub> ]		$mg/m^3$	703	599	651
average boiler water output temperature		°C	77,8	78,3	78,1
average boiler water input temperature		°C	70,0	70,0	70,0
average boiler water temperature rise	$N$	°C	7,8	8,3	8,1
water flow rate	$M_w$	$kg/h$	300	288	294
water heat output	$P_w$	$kW$	2,8	2,8	2,8
space heat output	$P_{SH}$	$kW$	1,6	1,5	1,6
total heat output	$P$	$kW$	4,5	4,3	4,4

Dust emission: test A	$mg/MJ$	16,5	16,0	16,3
test B	$mg/MJ$	19,1	14,9	17,0
test C	$mg/MJ$	18,2	17,2	17,7
test D	$mg/MJ$	18,3	20,2	19,3
average	$mg/MJ$	18,0	17,1	17,6
Dust emission (at 13% O <sub>2</sub> ): test A	$mg/m^3$	24,7	24,1	24,4
test B	$mg/m^3$	28,7	22,4	25,6
test C	$mg/m^3$	27,3	25,8	26,6
test D	$mg/m^3$	27,5	30,3	28,9
average	$mg/m^3$	27,1	25,6	26,4
NOx	$ppm$	52	56	54
NOx (as NO <sub>2</sub> )	$mg/MJ$	73	74	74
NOx (as NO <sub>2</sub> at 13% O <sub>2</sub> )	$mg/m^3$	109	111	110
THC (as propane)	$ppm$	3,9	3,1	3,5
OGC (as C)	$mg/MJ$	4,7	3,5	4,1
OGC (as C at 13% O <sub>2</sub> )	$mg/m^3$	7,0	5,2	6,1

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## STATEMENTS OF THE TEST RESULTS

The requirements for CO, NO<sub>x</sub>, OGC and dust emissions and for efficiency of Austrian 15a B-VG, German BIMSChv, French Flamme Verte and Swiss LRV for appliances hand fired by wood are the following.

Austrian 15a B-VG

Nominal heat power	
	[mg/MJ]
CO	500
NO <sub>x</sub>	100
OGC	30
dust	25
efficiency	80

Reduced heat power	
	[mg/MJ]
CO	750
OGC	30
efficiency	80

German BIMSChv limits (at 13% O<sub>2</sub>)

CO [mg/m <sup>3</sup> ]	dust [mg/m <sup>3</sup> ]	efficiency [%]
200	20	90

Swiss LRV limits (at 13% O<sub>2</sub>)

CO [mg/m <sup>3</sup> ]	dust [mg/m <sup>3</sup> ]
500	40

French Flamme Verte limits (at 13% O<sub>2</sub>)

stars	CO [mg/m <sup>3</sup> ]	dust [mg/m <sup>3</sup> ]	efficiency [%]
5	500	90	85
6	375	40	87
7	250	30	90

The appliance **PPF 18 of Klover** fulfils the requirements of

- Austrian 15a BV-G
- German BIMSChv
- Swiss LRV limits
- Flamme Verte (7 stars).

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## MEASURING DEVICES

The requirements of the measuring instruments are fulfilled.

Before each qualified measuring analysers were calibrated with zero gas and calibration gas.

Parameter measured	principle	Company	range	uncertainty	Calibration gas
O <sub>2</sub>	paramagnetic	MRU	0 – 21%	±0.1%	0 – 2,5 – 9,0- - 21%
CO <sub>2</sub>	infra-red	MRU	0 – 20 %	±1%	0 – 9 – 18 %
CO	infra-red	MRU	0 – 32000 ppm	±2%	0 – 450 – 2500 - 4500 ppm
NO <sub>x</sub>	infra-red	MRU	0 – 500 ppm	±2%	0 – 50 – 250 – 450 ppm
OGC	FID	Ratfisch	0 -100 ppm	±2%	0 – 82 ppm propane
static pressure	--	MRU	0 – 25 Pa	±0,25 Pa	0 – 20 Pa
temperature: ambient room flue gas surface touchable areas	K thermocouple K thermocouple T thermocouple K thermocouple	National Instruments	10 – 50°C 20 – 1000°C 20 – 250°C 20 – 250 °C	±0.5°C ±2°C ±1°C ±1°C	-- -- -- --
cross-draught	heated thermistor	Schmidt Feintechnik	0 – 20 m/s	±0.1 m/s	--
mass: fuel consumption fuel load	balance balance	SBP SBP	0 – 1500 kg 0 – 10 kg	±20 g ±0,5 g	-- --

All data were continuously recorded with data logger at intervals of 5 seconds. All raw data is stored for 10 years.

## FUEL DATA

Specifications of the test fuel used:

	nominal heat output test
Fuel	wood pellet
Moisture content [%]	6,0
Lower calorific value [KJ/Kg]	17861
Carbon content [% on dry basis]	46,8
Sulphur content [% on dry basis]	0,005
Hydrogen [% on dry basis]	5,7
Size: length [mm] diameter [mm]	12 – 30 (at the origin) 6,0